

# Supporting the optimal design and operation of CO<sub>2</sub> capture in industrial facilities with time-resolved models

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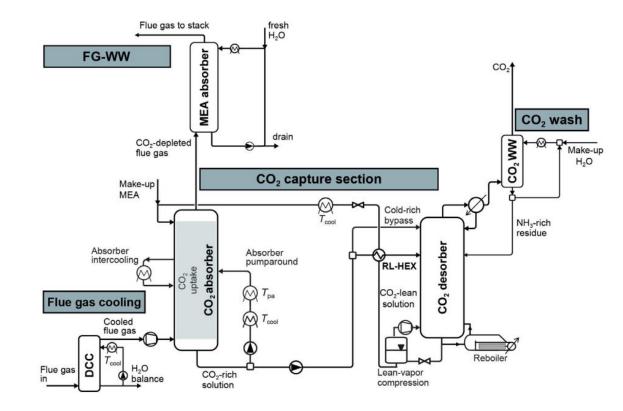


# Traditional techno-economic analysis lacks longer temporal resolution

The assessment and design of CCS technologies involve:

- Process simulations
- Techno-economic framework

Under the assumption that the operations and economic framework are static or dynamic with short time horizon

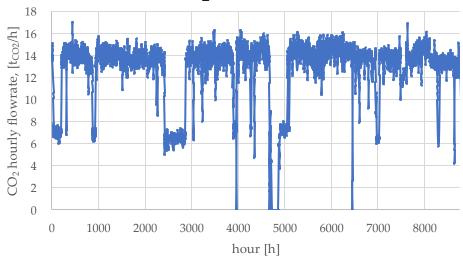




Source: Weimann, L., Dubbink, G., van der Ham, L., & Gazzani, M. (2023). A thermodynamic-based mixed-integer linear model of post-combustion carbon capture for reliable use in energy system optimisation. *Applied Energy*, 336. https://doi.org/10.1016/j.apenergy.2023.120738



#### Emission profile of a WtE

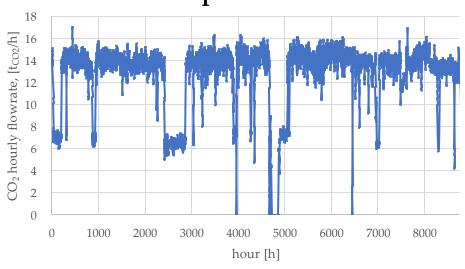




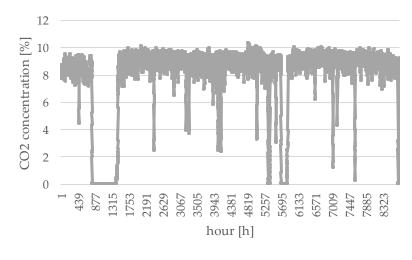




Emission profile of a WtE



#### CO<sub>2</sub> concentration in a WtE

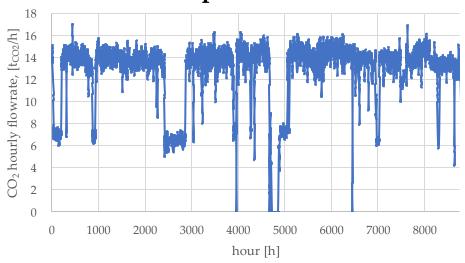




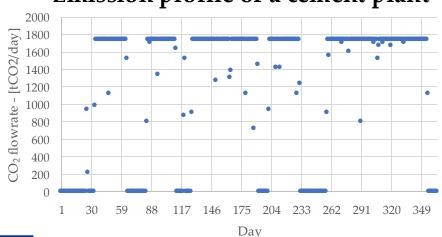




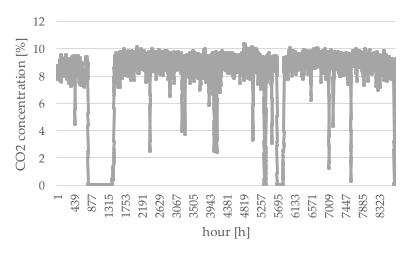
#### Emission profile of a WtE



#### Emission profile of a cement plant



#### CO<sub>2</sub> concentration in a WtE

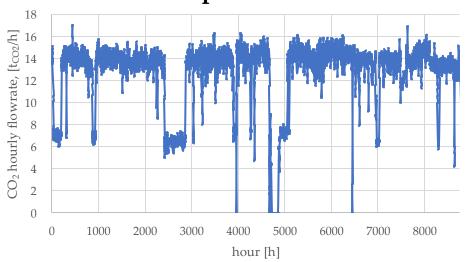




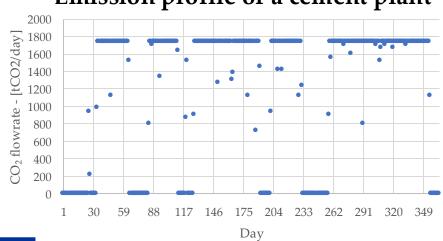




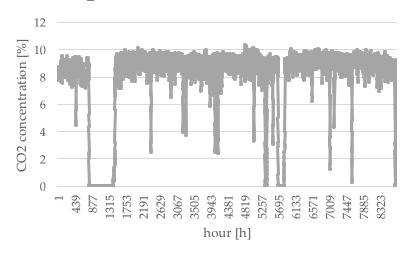
Emission profile of a WtE



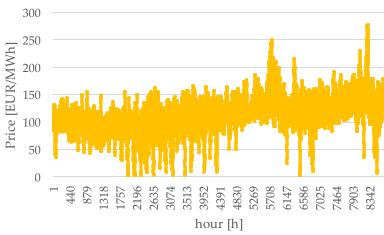
#### Emission profile of a cement plant



#### CO<sub>2</sub> concentration in a WtE



#### **Electricity price**

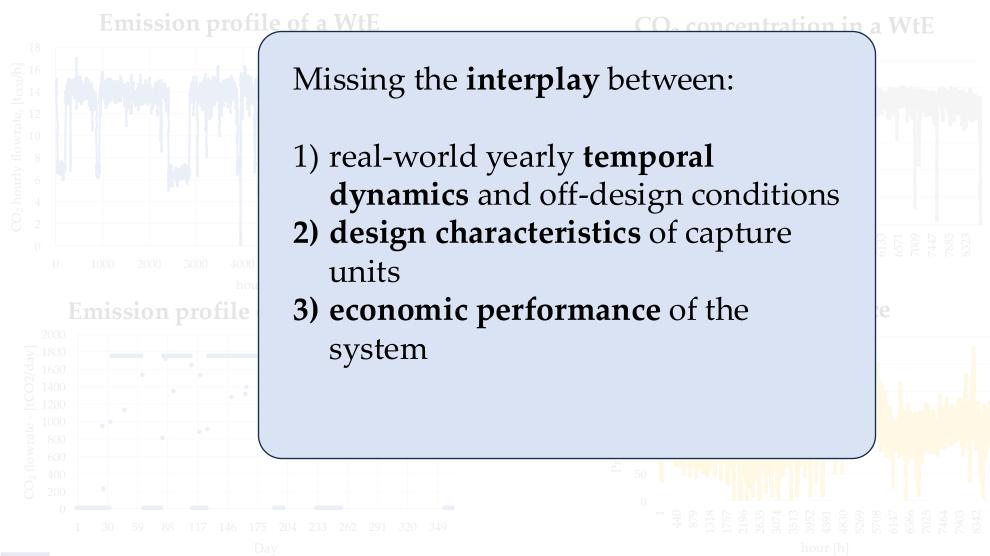








# In reality, CCS operates under dynamic conditions









# Can time-resolved models support the assessment of CO<sub>2</sub> capture technologies?







### Overview of the presentation

Modeling framework

Capture technologies and industries

Results

Conclusions







### Modeling framework - needs

Requirements of the modeling framework:

- handle ~100′000 variables or more for time resolution
- keep the physical fidelity to the process
- Identify optimal design and operating conditions







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Mixed integer linear programming (MILP)













Process simulations rate-based in ASPEN On- and off- design







Process simulations rate-based in ASPEN On- and off- design

Linear regression

Piecewise linear carbon capture model







# MILP framework – yearly time horizon, hourly resolution

Process simulations rate-based in ASPEN On- and off- design

Linear regression

Piecewise linear carbon capture model

- CO<sub>2</sub> concentration profile
- Real-world industrial production profiles
- Electricty prices
- District heating demand
- Interaction with other technologies (e.g. industrial boilers, heat pumps etc.)







### Main optimization variables and parameters

#### **Variables**

- Selection: capture technology
- Design: capture unit size
- Operation: portion of flue gas treated every hour

#### **Parameters**

- CAPEX as function of
  - size
  - design CO<sub>2</sub> concentration
- Energy input as function of
  - CO<sub>2</sub> processed
  - design CO<sub>2</sub> concentration
  - hourly CO<sub>2</sub> concentration





# Capture technologies



# Industry

Waste to energy

**Cement** 

[1]: Weimann, L., Dubbink, G., van der Ham, L., & Gazzani, M. (2023). A thermodynamic-based mixed-integer linear model of post-combustion carbon capture for reliable use in energy system optimisation. *Applied Energy*, 336. https://doi.org/10.1016/j.apenergy.2023.120738





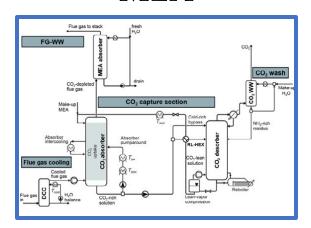
# Industry

# Capture technologies

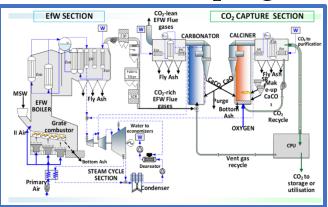


#### MEA [1]

Waste to energy



#### Calcium looping



#### **Cement**

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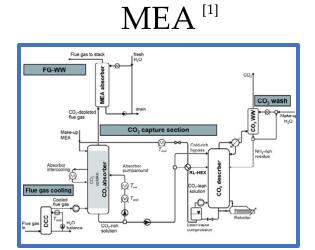


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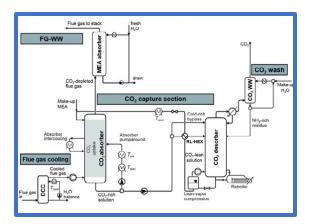


Waste to energy

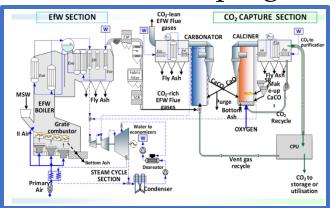
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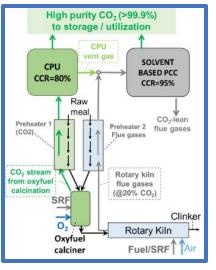


 $MEA^{[1]}$ 



Calcium looping





Partial oxyfuel only/plus PCC

[1]: Weimann, L., Dubbink, G., van der Ham, L., & Gazzani, M. (2023). A thermodynamic-based mixed-integer linear model of post-combustion carbon capture for reliable use in energy system optimisation. *Applied Energy*, 336. https://doi.org/10.1016/j.apenergy.2023.120738



Industry

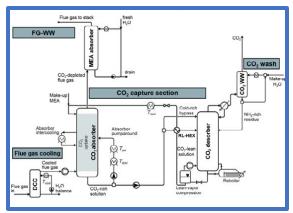


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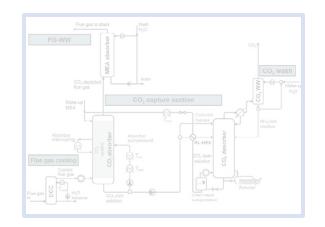


#### $MEA^{[1]}$

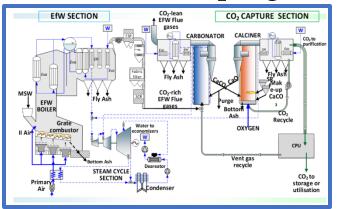
Waste to energy

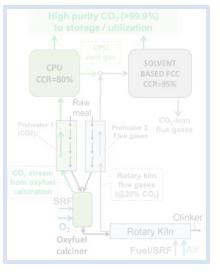






Calcium looping





Partial oxyfuel only/plus PCC

Cement

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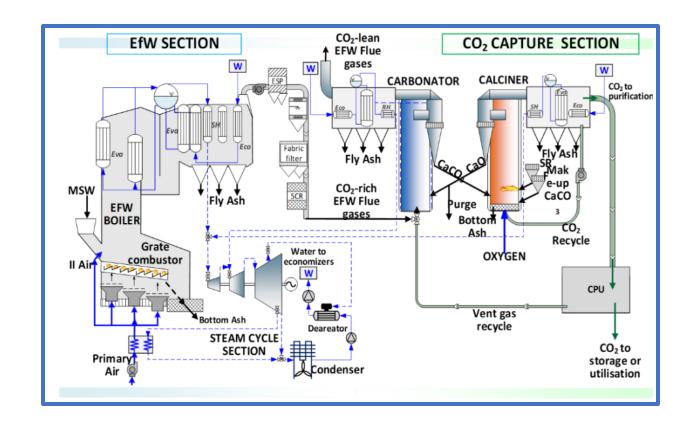


Industry





# Calcium looping for waste-to-energy







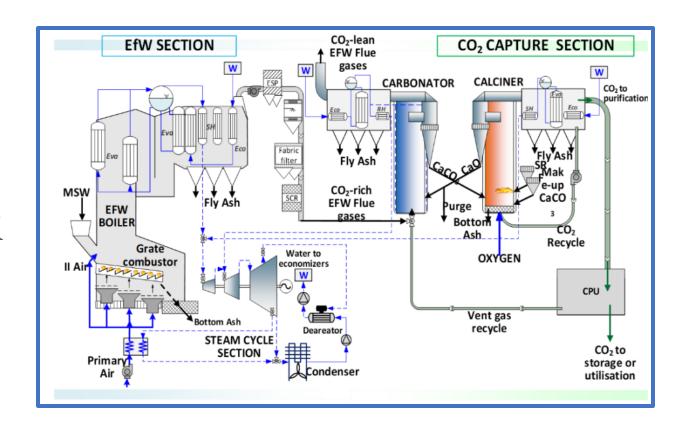


# Calcium looping for waste-to-energy

We performed **multiple** ASPEN **simulations** of CaL in a WtE facility:

- 3 plant sizes: small, mid, big
- 2 target CO<sub>2</sub> concentrations: 8% and 10%

KPIs: CAPEX, OPEX, net el. production, fuel consumption





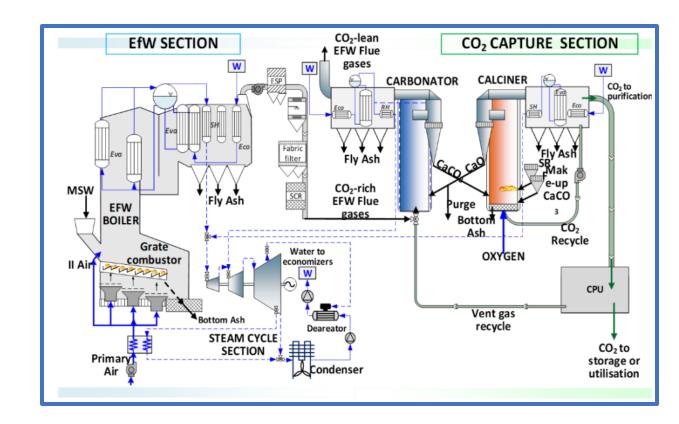




# Calcium looping for waste-to-energy

#### We simulated **off-design** conditions:

- Flowrate variation: ±7% compared to baseline
- CO<sub>2</sub> concentration variation: ±1% compared to baseline



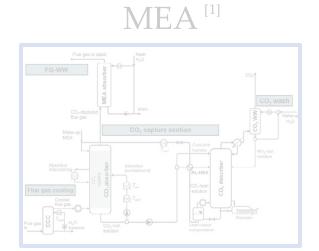




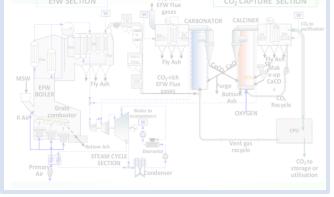
# Capture technologies



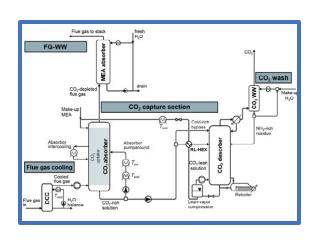
# Waste energy

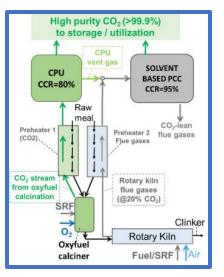


# Calcium looping



MEA [1]





Partial oxyfuel only/ plus PCC

**Cement** 

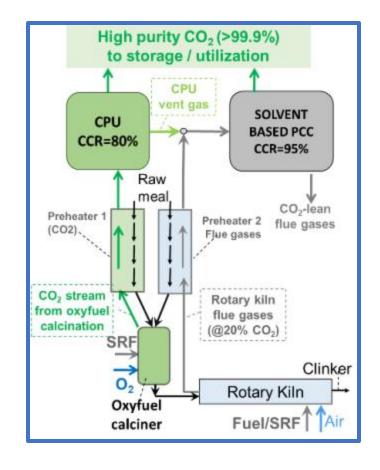
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# Partial oxyfuel with PCC for cement







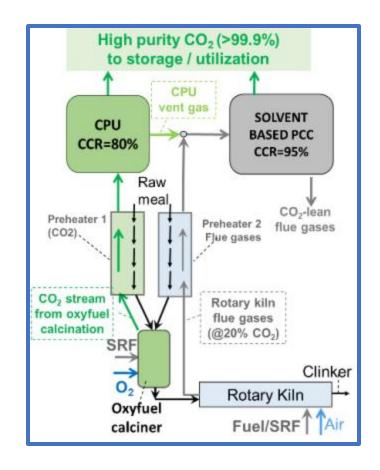


# Partial oxyfuel with PCC for cement

We performed **multiple** ASPEN **simulations** of the partial oxyfuel/hybrid oxyfuel+PCC capture options:

- 2 plant sizes: 1800 and 3000 tpd clinker
- Oxyfuel only, oxyfuel with PCC

KPIs: CAPEX, OPEX, el. consumption, extra fuel consumption





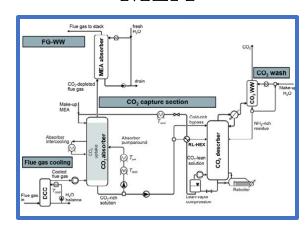


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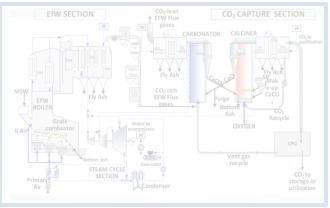


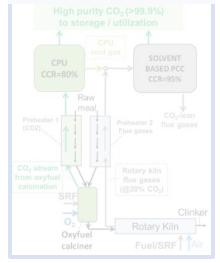
#### MEA [1]

Waste to energy



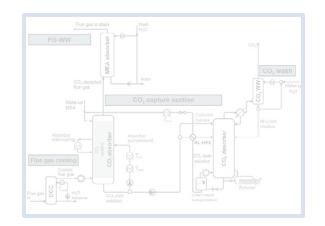






Partial oxyfuel only/plus PCC

MEA [1]



Cement

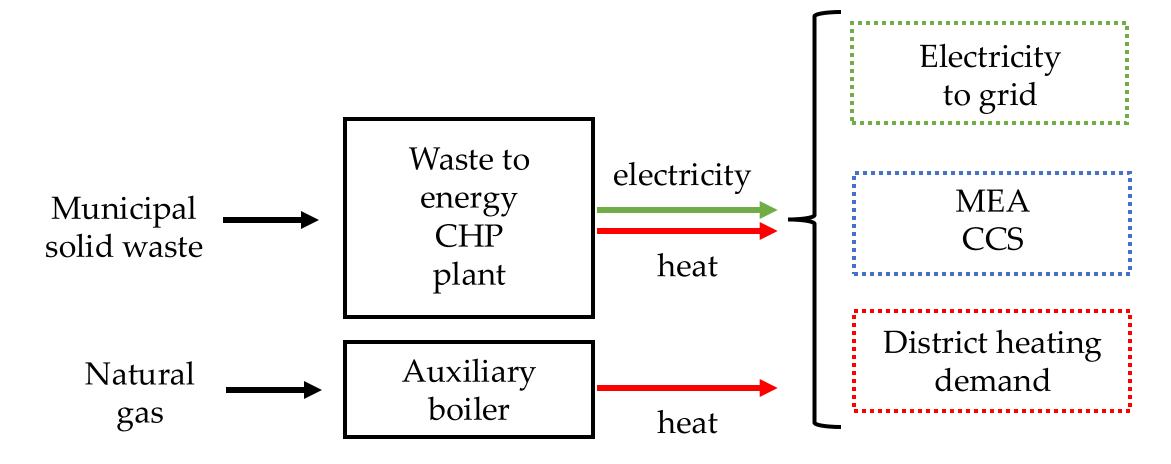
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# Application to a combined heat and power WtE with MEA

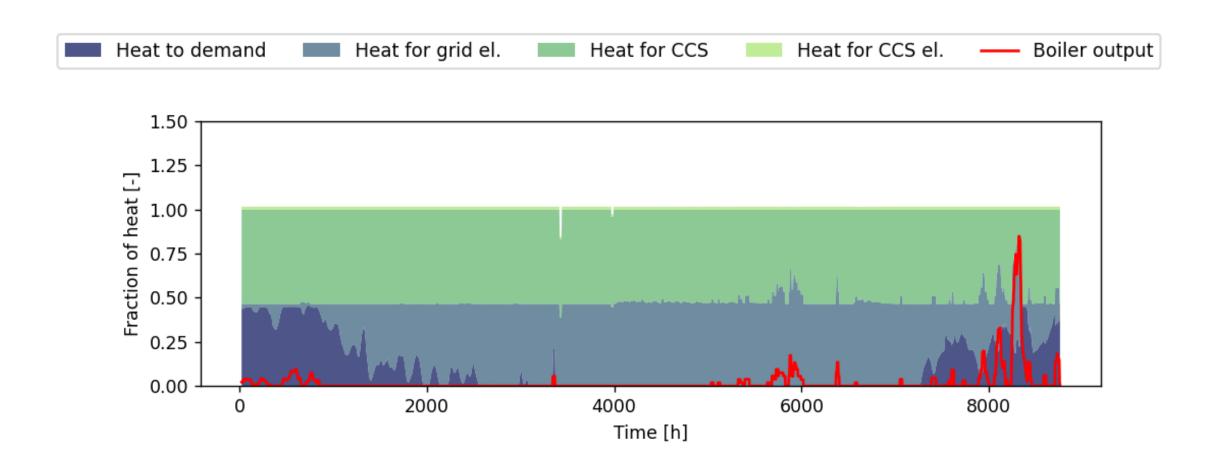








# Optimal heat usage in the WtE throughout the year...

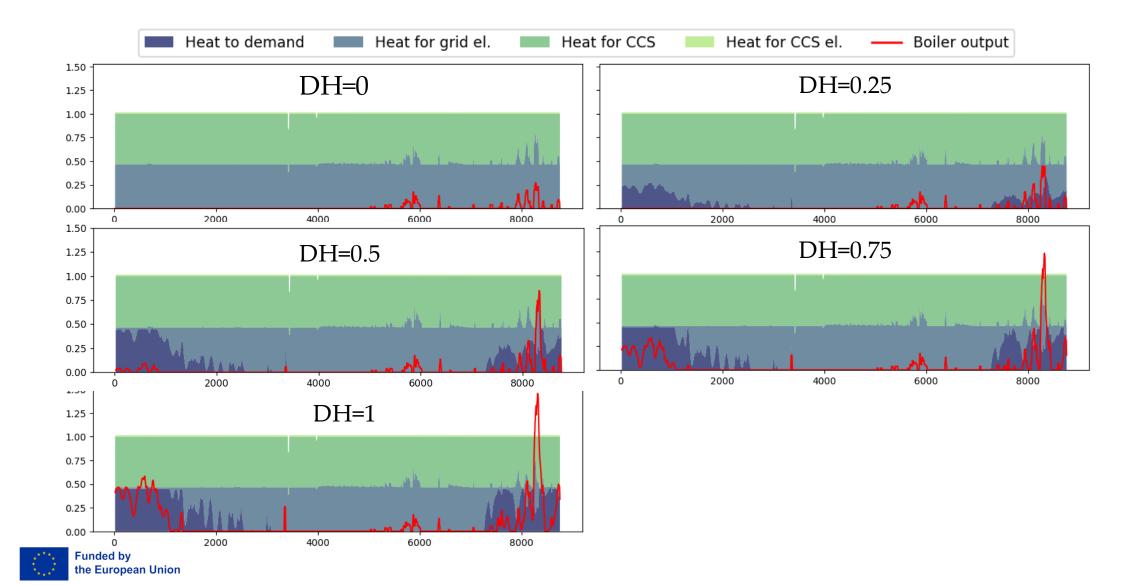








# ...with increasing district heating (DH) demand



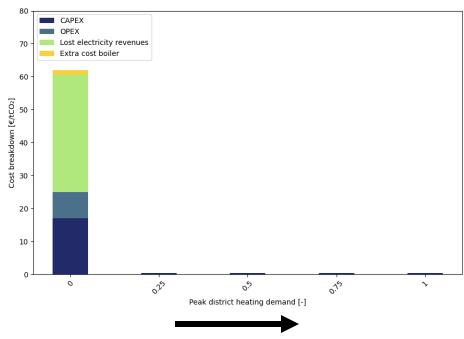




### Impact of increasing DH demand on MEA costs

#### Time-resolved analysis

Cost of capture



Increasing DH demand

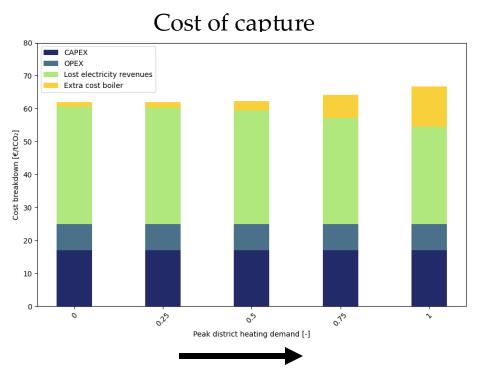






# Assessing the opportunity cost of MEA in WtE

#### Time-resolved analysis





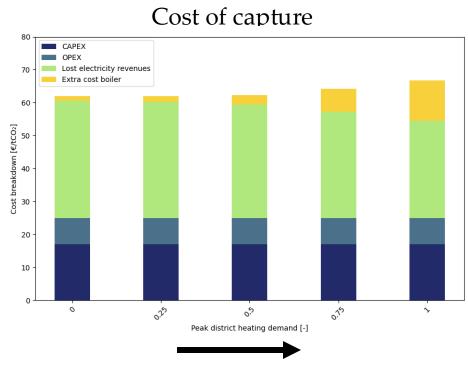






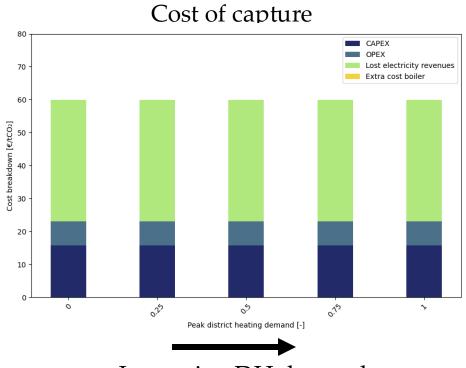
# Assessing the opportunity cost of MEA in WtE

#### Time-resolved analysis



Increasing DH demand

#### Static analysis



Increasing DH demand

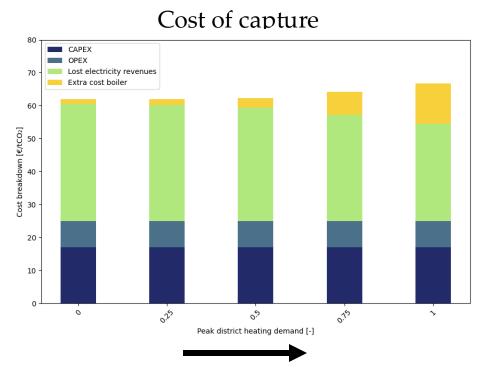






# Assessing the opportunity cost of MEA in WtE

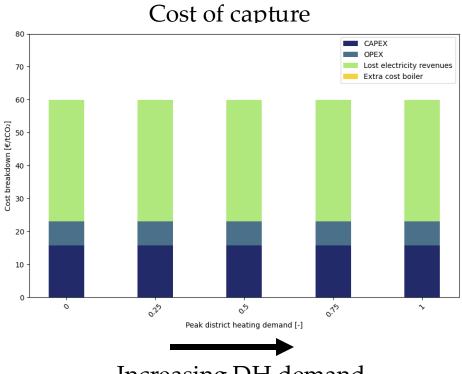
#### Time-resolved analysis



Increasing DH demand

Optimal CCS size: 88%

#### Static analysis



Increasing DH demand

Optimal CCS size: 100%



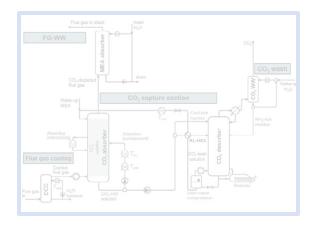


# Capture technologies

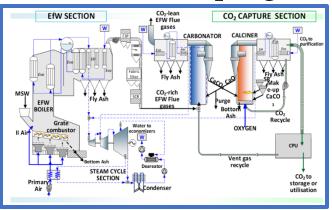


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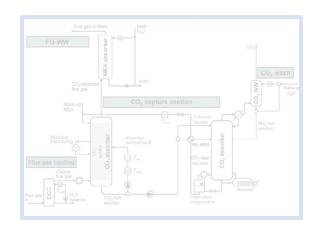
MEA [1]



Calcium looping



MEA [1]



High purity CO<sub>2</sub> (>99.9%)
to storage / utilization

CPU
vent gas

SOLVENT
BASED PCC
CCR=95%

Raw
meal
Preheater 2
Flue gases

Flue gases

CO<sub>2</sub> tream
from oxyfuel
calcination

Rotary Kiln
Gases

Clinker
O2
Clinker
Preheater 2
Flue gases
Flue gases

Rotary Kiln
Flue Gases

Clinker
O2
Clinker
O2
Clinker
O2
Clinker
O3
Clinker
O4
Fuel/SRF
Air

Partial oxyfuel only/plus PCC

[1]: Weimann, L., Dubbink, G., van der Ham, L., & Gazzani, M. (2023). A thermodynamic-based mixed-integer linear model of post-combustion carbon capture for reliable use in energy system optimisation. *Applied Energy*, 336. https://doi.org/10.1016/j.apenergy.2023.120738





Waste

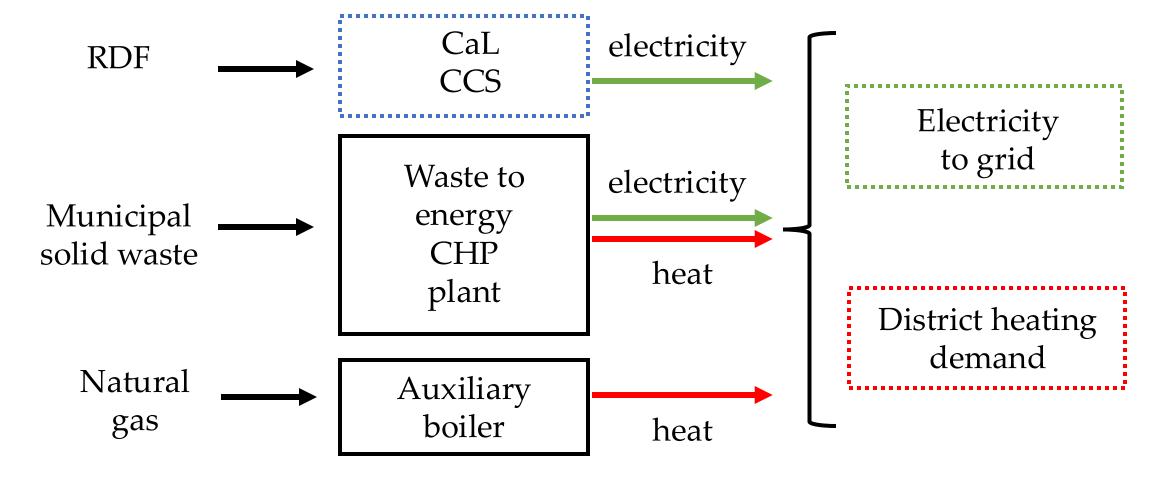
to

energy

Cement



# Application to a combined heat and power WtE with calcium looping



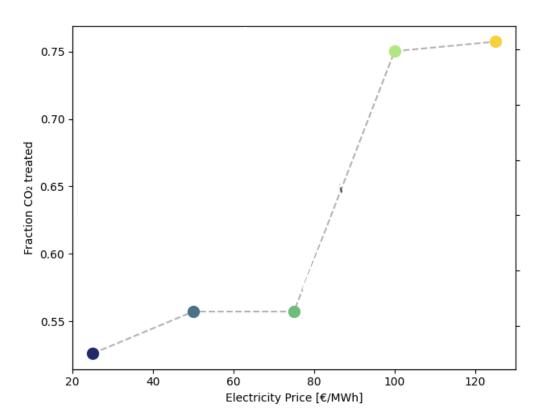






# Calcium looping in WtE with varying el. prices

Optimal CaL size (fraction of peak)



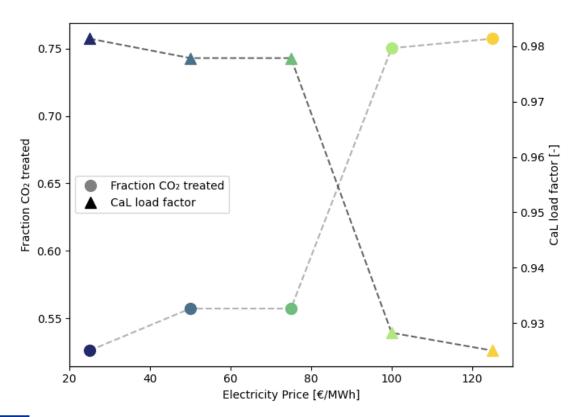






# Calcium looping in WtE with varying el. prices

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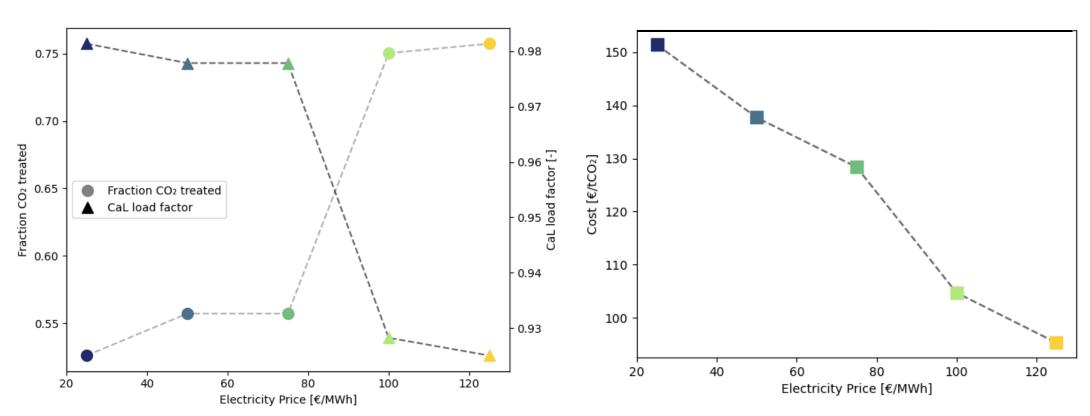




# Calcium looping in WtE with varying el. prices



Cost of capture









#### **Conclusions**

- The impact of the time-resolution changes with the industry and the characteristics of the plant
- Time-resolved models support the assessment of capture technologies in technology selection, design and operation
- They help quantifying trade-offs and improving the economics of the system









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- Time-resolved models support the assessment of capture technologies in technology selection, design and operation
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Any questions?

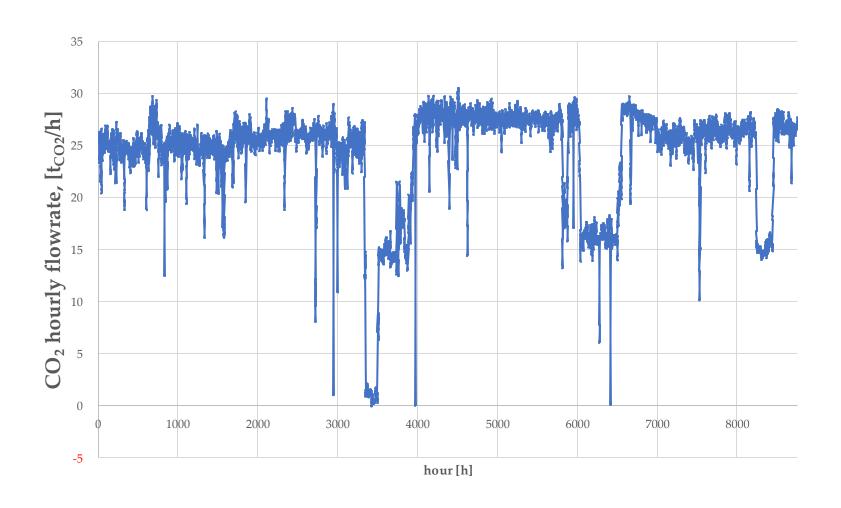








# WtE profile







Funded by the European Union



# Cement plants: capture technology selection

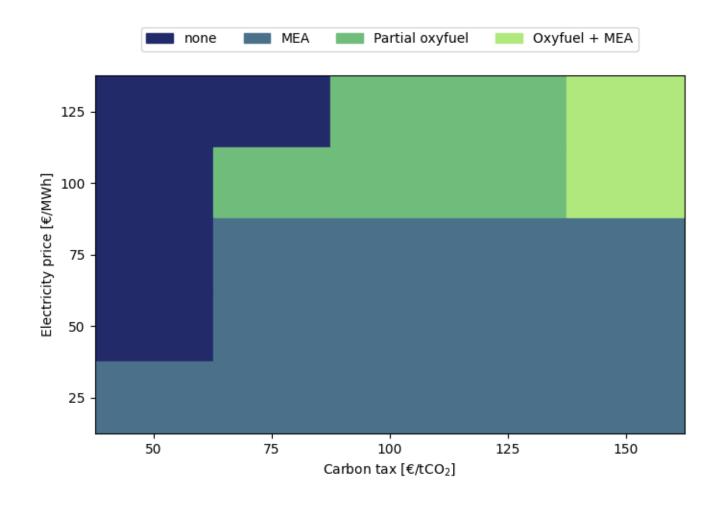








# Cement plants: capture technology selection

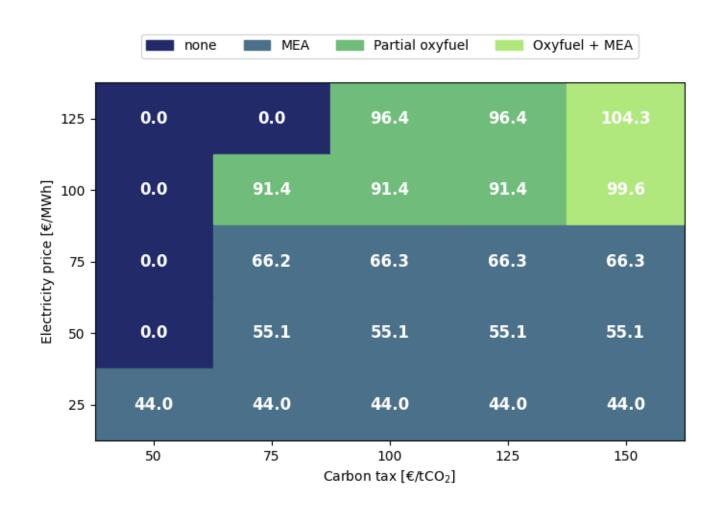








### Cement plants: capture technology selection



Cost of capture in EUR/tCO<sub>2</sub>







# Capture technologies

Industry

Waste to energy

MEA [1]

Calcium looping

**Cement** 

MEA [1]

Partial oxyfuel only/ plus MEA

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